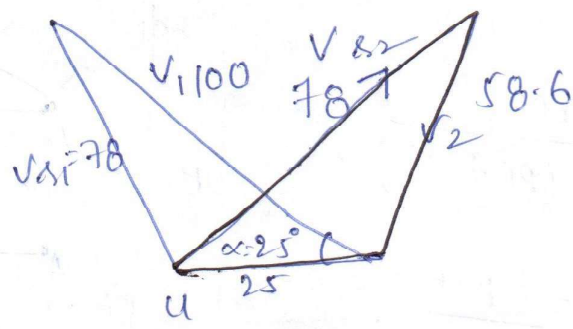


G-14
16

Axial flow T. Turbine



- $V_1 = 100 \text{ m/sec}$ ✓
- $u = 25$ ✓
- $\alpha = 25^\circ$ ✓
- $V_{f1} = V_{f2}$ ✓
- $V_{f1} = V_{f2}$ ✓

Sp work J/kg = _____ ?

$$RP = \frac{\rho Q [V_{w1} + V_{w2}] u}{m}$$

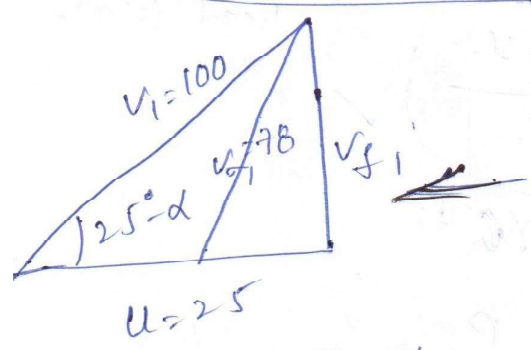
$$RP = \left(\frac{J}{\text{sec}} \right) \left(\frac{\text{kg}}{\text{kg}} \right)$$

$$\frac{J}{\text{kg}} = \frac{RP}{\left(\frac{\text{kg}}{\text{sec}} \right)}$$

Sp work J/kg =

$$\frac{[V_{w1} + V_{w2}] u}{m}$$

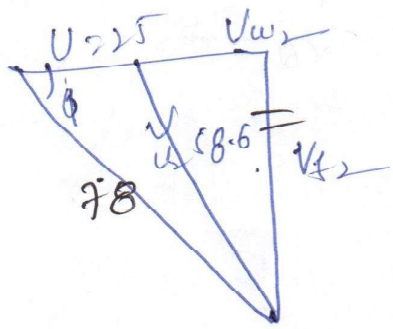
$$V_{w2} = \sqrt{V_2^2 - V_{f2}^2}$$



$$V_{w1} = V_1 \cos 25$$

$$V_{w1} = 100 \times \cos 25$$

$$V_{w1} = 90.63 \text{ m/s}$$



$$V_{f2} = V_{f1} = V_1 \sin \alpha$$

$$= 100 \sin 25$$

$$V_{f2} = 42.26 \text{ m/s}$$

$$V_{f2} = V_1 \sin 25 \Rightarrow V_{w2} = \sqrt{58.6^2 - (100 \sin 25)^2}$$

$$= V_{w2} = 40.5 \text{ m/sec}$$

$$V_{w2} = \underline{40.7 \text{ m/s}}$$

$$\text{Sp. work} = [V_{w1} + V_{w2}] u$$

$$= [90.63 + 40.5] \times 25$$

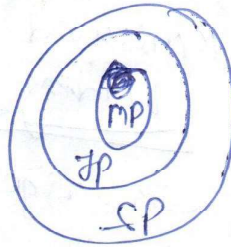
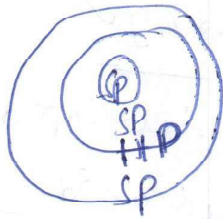
$$= \underline{3278 \text{ J/kg}} \rightarrow \underline{3278 \text{ kJ/kg}} \checkmark$$

∞ Pump ∞

① Centrifugal pump :- \leftrightarrow Francis turbine

\rightarrow (F.T) \approx (C.F pump)

Radial entry



JP = Impeller power

MP = manometric power

- SP \rightarrow Rating

$$\rightarrow (R.P)_{R-T} = JP = \text{Impeller power} = \rho Q [V_{w2} u_2 - V_{w1} u_1]$$

$$\rightarrow HP = \text{manometric power} = \rho Q H_m = \rho Q V_{w2} u_2$$

$$\eta_{\text{mech}} = \frac{JP}{IP}, \quad \eta_{\text{mano}} = \frac{MP}{IP}, \quad \eta_{\text{vol}} = \frac{Q}{Q + A\omega}$$

$$\eta_{\text{mano}} = \frac{g H_m}{V_{w2} u_2}$$

$$\eta_{\text{Overall}} = \eta_{\text{mech}} \times \eta_{\text{mano}} \times \eta_{\text{vol}}$$

Water exit whirl velocity is zero

$$\underline{V_{w2} = 0}$$

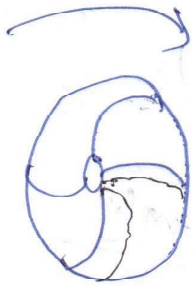
Water enters without whirl velocity
 $V_{w1} = 0$

→ manometric m.p power = $\gamma a + m$

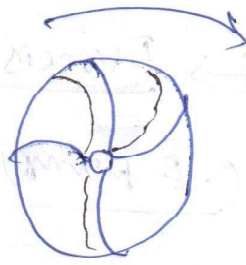
$$\eta_{\text{mech}} = \frac{FP}{S.P}, \quad \eta_{\text{mano}} = \frac{MP}{FP}$$

$$\eta_{\text{vol}} = \frac{Q - Aa}{Q} \left(\frac{Q}{a + Aa} \right)$$

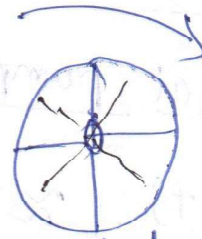
Types of blades in impeller :-



Forward blading ✓

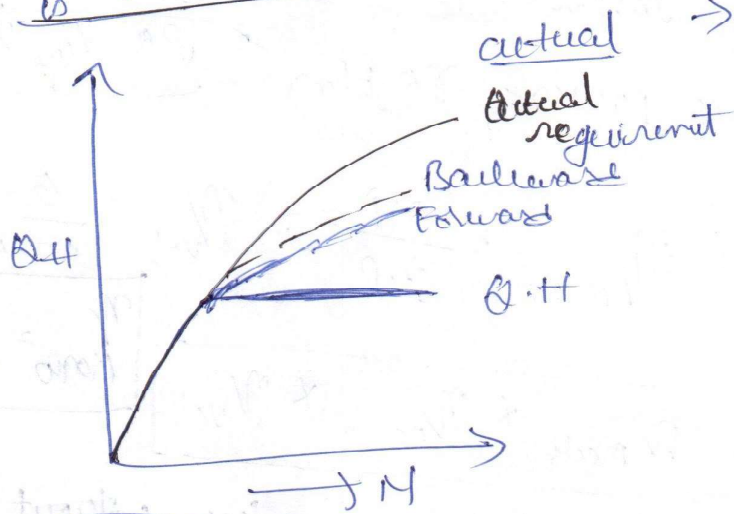


Backward blading ✓



Radial blading ✓

Note: Through discharge & head developed will be maximum for forward blading backward blading is most preferable

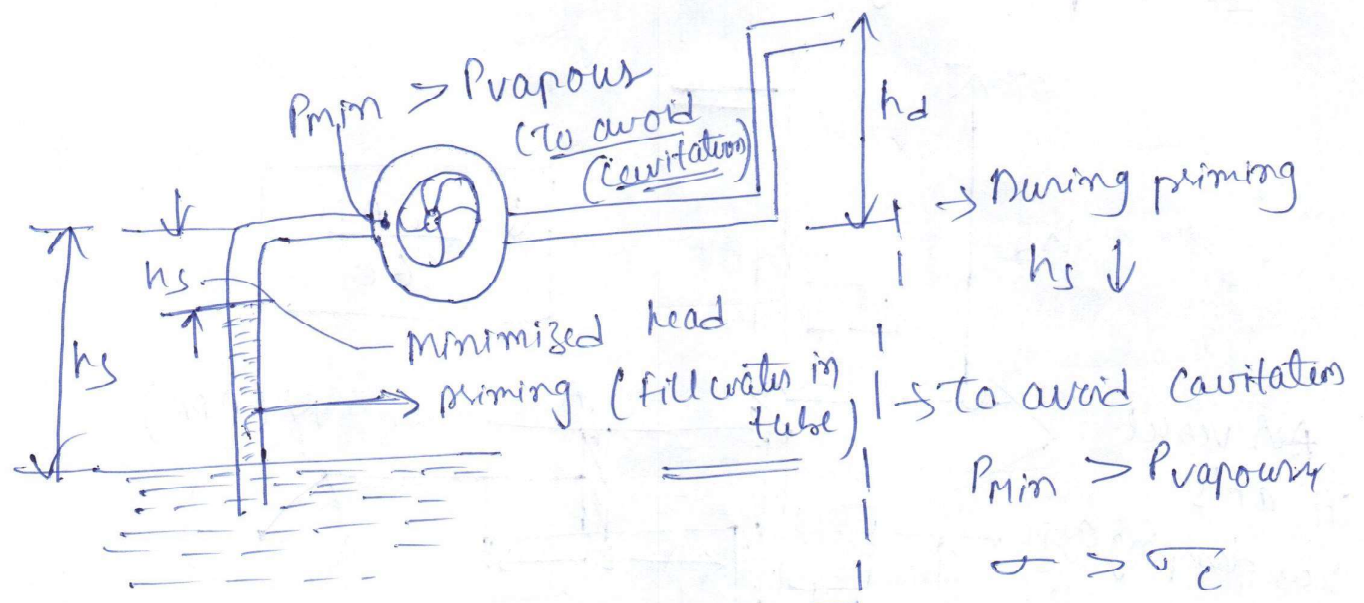


→ For Forward blading power required will be more when discharge & head will increase with slight high amt

NI \uparrow θ , $H \uparrow$
 after some speed $\theta, H \rightarrow$ asymptotes

Surging & stalling
 Area Compressor ✓

N.P.S.H (Net positive suction head):



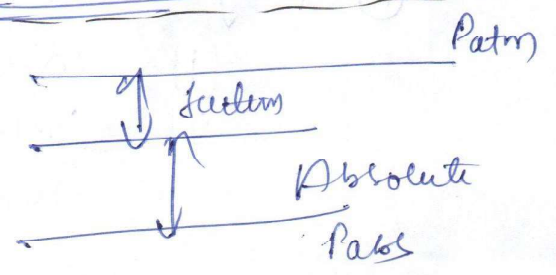
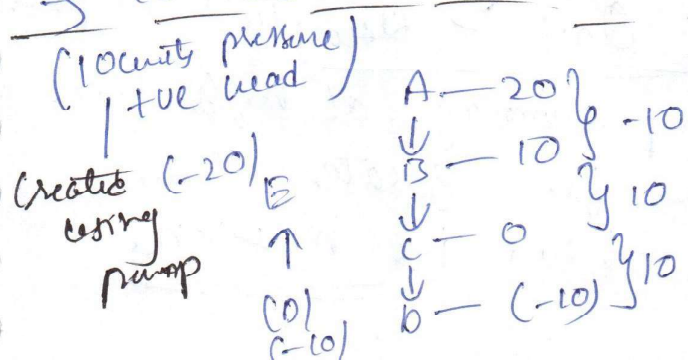
$\sigma > \sigma_c$
 $\sigma_c =$ Critical cavitation coefficient
 $\sigma =$ Thoma number
 $H_M =$ Failure head
 $H_M = h_s + h_d + h_{fs} + h_{fd}$

$$\sigma = \frac{NPSH}{H} \Rightarrow NPSH = \frac{P_{atm}}{\rho g} - h_s - h_{fs} - \frac{P_{vapour}}{\rho g} \text{ [Abs.]}$$

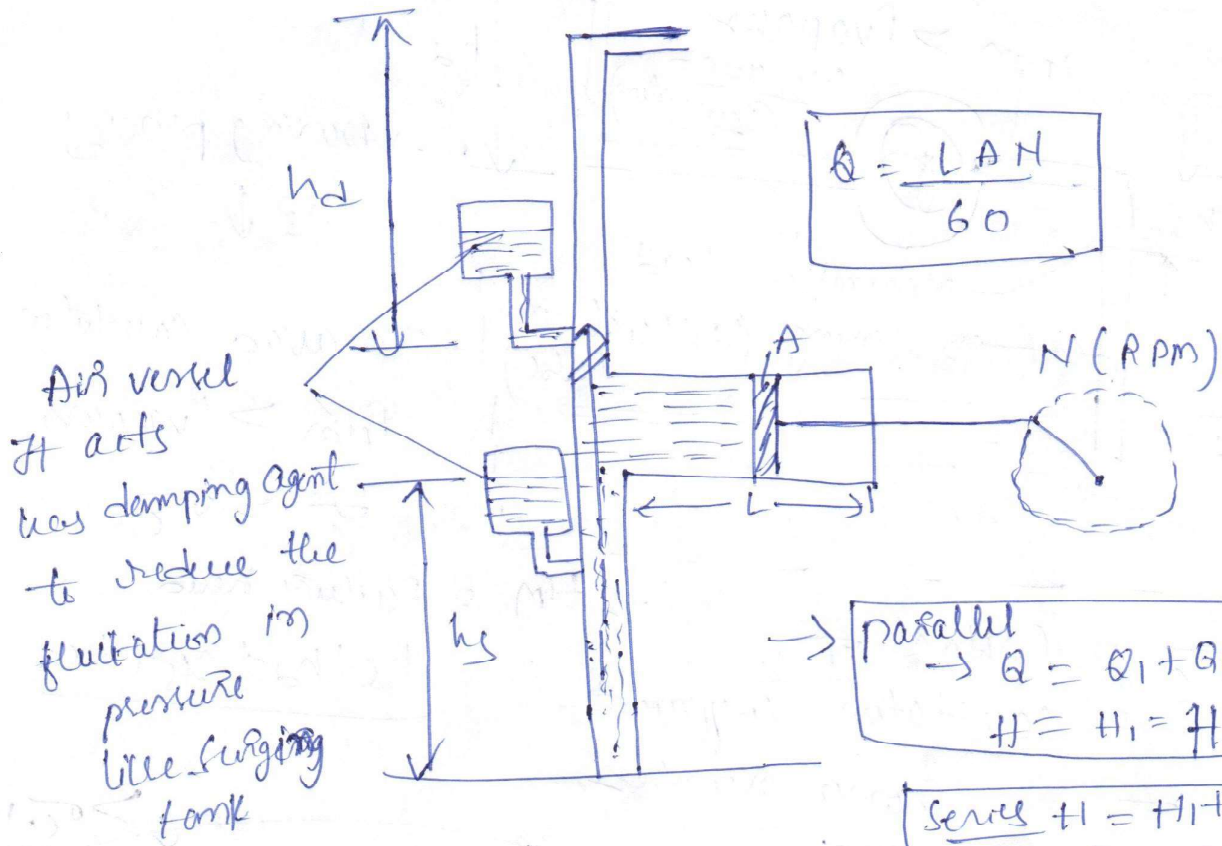
$$\Rightarrow NPSH = h_s + h_{fs} + \frac{P_{vapour}}{\rho g} \text{ [suction]}$$

$$\frac{NPSH}{H} > \sigma_c \Rightarrow NPSH > \sigma_c \times H$$

To avoid cavitation $\Rightarrow P_{min} > P_{vapour}$
 $\sigma > \sigma_c$



* Reciprocating pump :-



$$\text{Slip} = \frac{Q_{th} - Q_{act}}{Q_{th}} = 1 - \frac{Q_{act}}{Q_{th}}$$

$$\boxed{\text{Slip} = (1 - \eta)}$$

-ve slip
 $\hookrightarrow Q_{act} > Q_{th}$

$$\rightarrow Q = \frac{LAN}{60}$$

$$\frac{m^3}{sec} = \frac{vol}{stroke} \times \left(\frac{stroke}{rev} \right) \left(\frac{rev}{min} \right) \Big|_{60} = m^3/sec$$

Notes:

- ① Negative slip $\Rightarrow Q_{act} > Q_{th}$ will be possible
 - (i) when pump running at high speed
 - (ii) suction head for greater than delivery head i.e. $h_s > h_d$

α

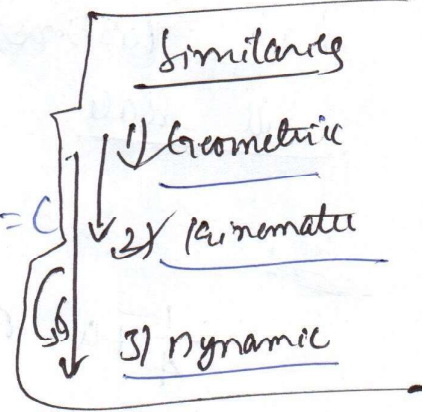
1st preference

Unit quantity \rightarrow Unit speed $Nu = \frac{N}{\sqrt{H}}$, $Qu = \frac{Q}{\sqrt{H}}$

$$Pu = \frac{P}{H^{3/2}}$$

Model study :-

$$\frac{\sqrt{H}}{DN} = C ; \quad \frac{Q}{D^3 N} = C ; \quad \frac{P}{D^5 N^3} = C$$



2

Specific speed \Rightarrow (Ns)

<u>Turbine</u>	<u>Pump</u>
$\frac{N \sqrt{P}}{H^{5/4}}$	$\frac{N \sqrt{Q}}{H^{3/4}}$

Ques

Q: If speed of centrifugal pump is double the power required to drive the pump will

Speed
Power

Case 1	Case 2
N	2N
P	P ₂

$$\rightarrow \left\{ \begin{aligned} P &\propto N^3 \quad \dots \quad \frac{P}{D^5 N^3} = C \\ \frac{P_1}{P_2} &= \left(\frac{N_1}{N_2}\right)^3 = 1 \quad P_2 = 8P_1 \end{aligned} \right.$$

(D₁ = D₂ = D)

geometric similarity

$$\left[\frac{P}{D^5 N^3} \right]_1 = \left[\frac{P}{D^5 N^3} \right]_2$$

then using the formula

$$P_2 = P_1 \left(\frac{N_2}{N_1} \right)^3 = P \left(\frac{2N}{N} \right)^3$$

$$\left(\frac{P}{D^5 N^3} \right) = C$$

P₂ = 8P

Q-06

A model of turbine working under a head of $\frac{1}{4}H$ of that under which full scale turbine works. The dia of model is $\frac{1}{2}$ of full scale. If N is RPM of model. RPM full scale will be ✓

Sol:

$\frac{1}{4}H$ of Full scale

N - (RPM model) R.P.M (F.S) = ?

$\frac{N}{2N} \rightarrow \frac{N/2}{4N}$ ✓

	F.S	Model
Head	$4H$	H
Dia	$2D$	D
R.P.M	$(M)?$	N

$\Rightarrow \frac{\sqrt{4H}}{2DN_1} = \frac{\sqrt{H}}{DN}$

$N_1 = N$ ✓

$\left(\frac{\sqrt{H}}{DN} \right)_{FS} = \left(\frac{\sqrt{H}}{DN} \right)_{mod}$

Q-10

A turbine working under head of 40m was developing a power of 100kw. If the head reduced to 20m the power developed in kW

Sol:

$H(m)$	40	20 ✓
$P(kw)$	1000	$(P_2)?$ ✓

$\frac{P_1}{H_1} = \left[\frac{P}{H^{3/2}} \right]$

$$\left[\frac{P}{H^{3/2}} \right]_1 = \left[\frac{P}{H^{3/2}} \right]_2$$

$$\rightarrow P_2 = 1000 \times \left(\frac{20}{40} \right)^{3/2}$$

$$= \frac{1000}{2^{1.5}} \approx \underline{\underline{354 \text{ kW}}} \quad (354 \text{ kW})$$

Q-05

A turbine working under head of 40m when running at 1000 R.P.M was developed 300kW for initial testing a 1:4 scale model of turbine working under head of 10m can develop power of (P_2) ?

Q.

	FS	Model
Head (H)	40	10
Power (P)	300	(P_2) ?
R.P.M (N)	1000	
Scale (D)	4D	D

Unless the dynamic & kinematic ratio is maintained the given ratio must be taken as geometric ratio.

P, H, D (Power, head diameter)

$$\frac{\sqrt{H}}{DN} = C \rightarrow \sqrt{H} \propto DN$$

$$\therefore \frac{P}{D^5 N^3} = C \Rightarrow \frac{P}{D^2 (DN)^3} = C$$

$$\boxed{\frac{P}{D^2 \times H^{3/2}} = C} \Rightarrow \left[\frac{P}{D^2 \times H^{3/2}} \right]_{FS} = \left[\frac{P}{D^2 \times H^{3/2}} \right]_{\text{model}}$$

$$\frac{300}{(40)^2 (40)^{3/2}} = \frac{P_2}{(10)^2 \times (4)^{3/2}}$$

$$P_2 = \frac{300}{16 \times 4^{1.5}} = \underline{\underline{2.34 \text{ kW}}}$$

Gate
ES

Given

Failure head = 40m — (H)

Atm. pressure head = 10.5m — $\left(\frac{P_{atm}}{\rho g}\right)$

vapour pressure head = 2.5 → $\left(\frac{P_{vapour}}{\rho g}\right)$

Cavitation coefficient = 0.15 (σ_c)

More height at which turbine machine can set above tail race level!

Q.

$$NPSH = \left(\frac{P_{atm}}{\rho g}\right) - \left(H_s + \overset{\uparrow}{h_{fs}} + \frac{P_{vapour}}{\rho g}\right)$$

$$\sigma_c \cdot H \leq NPSH$$

$$\sigma_c \cdot H \leq NPSH$$

$$\rightarrow \sigma_c \cdot H \leq 10.5 - 2.5 - H_s$$

$$\rightarrow 10.5 - h_s - 2.5 \geq 0.15 \times 40$$

$$h_s \leq 2 \text{ m} \checkmark$$

When ↓ V · DT

$$z + \frac{P}{\rho g} + \frac{v^2}{2g} = C$$

When V ↓ $\frac{v^2}{2g}$ ↓ $\frac{P}{\rho g}$ ↑

At exit of turbine

$$P < P_{atm}$$

Hence draft tube

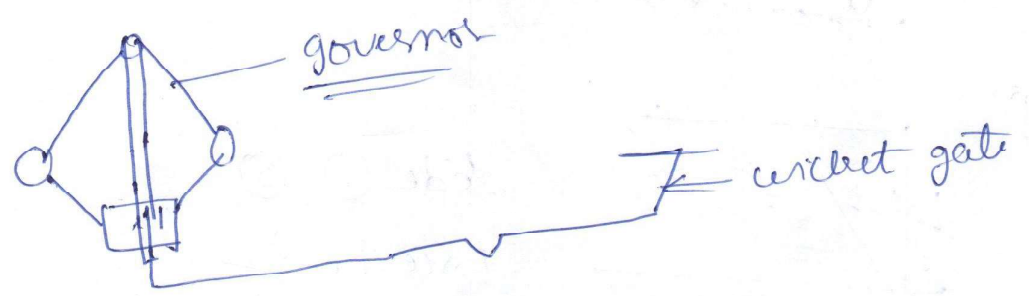
used to increase pressure energy ←

* Run away speed :- of turbine.

→ Run away speed of a turbine is a max. m speed that a turbine can experience under no load condition with wicket gate wide open (Maximum mass flow)

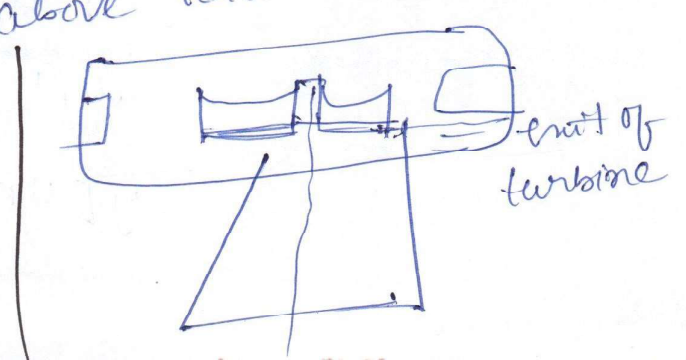
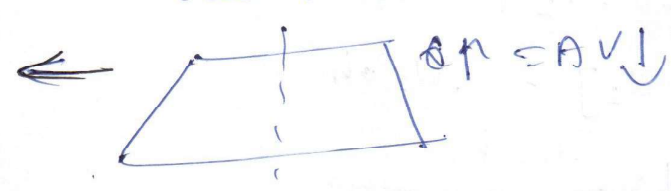
→ It is a structural integrity test in which governor is not present. It does not happen in reality.

→ In actual when maximum velocity & no load condition occurs, governor will act & gate will get be closed; so no load & wicket open gate will not happen simultaneously.



* Draft tube :-

Draft tube is required at exit of reaction turbine to convert large portion of its kinetic energy as waste into useful pressure energy, hence makes it possible to erect (install) the turbomachine above tail race level.

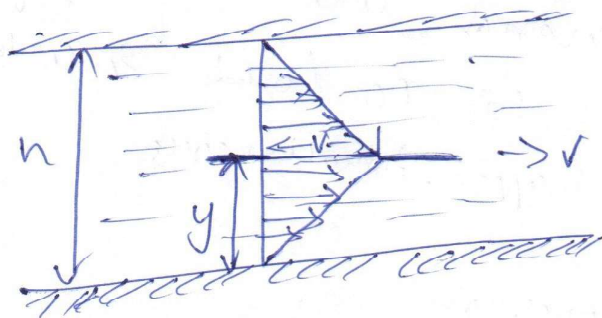


1) Through a very narrow gap of height h , a thin plate of large extent is pulled at a velocity v on the one side of viscosity μ_1 and on other side of viscosity μ_2

Calculate the position of the plate so that

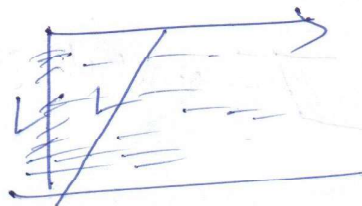
(i) The shear force on two sides of plate is equal $\Rightarrow F_1 = F_2$

(ii) The pull required to drag the plate is minimum



$$F = \frac{\mu A v}{y}$$

(i)



side (1) (2)

Force F_1 F_2

viscosity μ_1 μ_2

Area $A_1 = A_2 = A$

vel $v_1 = v_2 = v$

Dis $(h-y) = y$

$$\textcircled{1} F_1 = F_2 \Rightarrow \frac{\mu_1 A v}{(h-y)} = \frac{\mu_2 A v}{y}$$

$$\mu_1 y = \mu_2 (h-y)$$

$$y [\mu_1 + \mu_2] = \mu_2 h$$

$$y = \frac{\mu_2 h}{[\mu_1 + \mu_2]}$$

② ~~pull~~ pull

$$\rightarrow \frac{dp}{dy} = 0, \frac{d}{dy} \left[\frac{u_1 AV}{(h-y)} + \frac{u_2 AV}{y} \right] = 0$$

$$\rightarrow u_1 AV - \frac{1}{(h-y)^2} (-1) + u_2 AV \left(-\frac{1}{y^2} \right) = 0$$

$$\sqrt{\frac{u_1}{(h-y)^2}} = \frac{u_2}{y^2} \Rightarrow \frac{\sqrt{u_1}}{(h-y)} = \frac{\sqrt{u_2}}{y}$$

$$\sqrt{u_1} \cdot y = \sqrt{u_2} [h-y]$$

$$\sqrt{u_1} \cdot y + \sqrt{u_2} \cdot y = \sqrt{u_2} \cdot h$$

$$\boxed{y = \frac{\sqrt{u_2} \cdot h}{\sqrt{u_1} + \sqrt{u_2}}}$$

$$= y_2 \frac{\sqrt{u_2} \cdot h}{\sqrt{u_2} \left(1 + \frac{\sqrt{u_1}}{\sqrt{u_2}} \right)} = y_2 \frac{h}{\left(1 + \frac{\sqrt{u_1}}{\sqrt{u_2}} \right)}$$

P-43

(6)

$$P - 0.85 \rho_w \cdot g \cdot 0.6$$

$$- \rho_H g \cdot 0.1 = 0$$

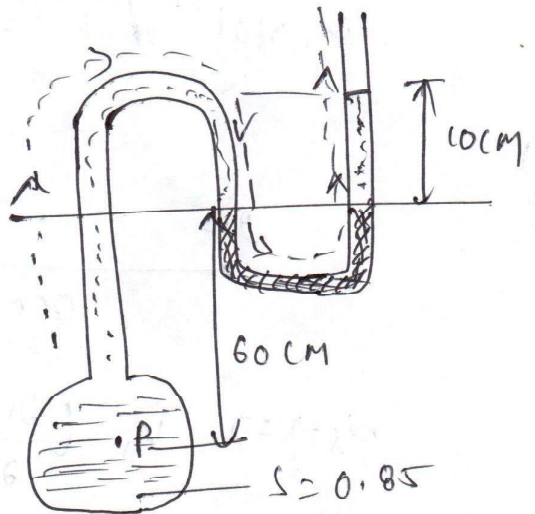
$$\rightarrow P - 0.85 \rho_w \cdot g \cdot 0.6 - \rho_H g \cdot 0.1$$

$$P = () + () = 18.31 \text{ kPa}$$

Ans

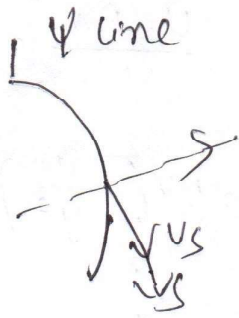
$$h = \frac{P}{\rho \cdot g}$$

$$= \frac{1.8 \times 10^3}{10^3 \times 9.81} = \underline{2.0}$$



P63
8)

23/7/17



$v = f [s, m, t]$

$$a_s = v_s \cdot \frac{\partial v_s}{\partial s} + v_n \cdot \frac{\partial v_n}{\partial t}$$

$$a_n = v_s \cdot \frac{\partial v_n}{\partial s} + v_n \cdot \frac{\partial v_n}{\partial t}$$

$v \text{ (measured)} \Rightarrow a_s = v_s \left(\frac{\partial v_s}{\partial s} \right)$

$a_n = \frac{v_s^2}{R}$

9

$v_s = 3 \text{ m/sec}$

$R = 9 \text{ m}$

$\frac{\partial v_s}{\partial s} = \frac{1}{3} \text{ m/sec} \cdot \frac{1}{\text{m}}$

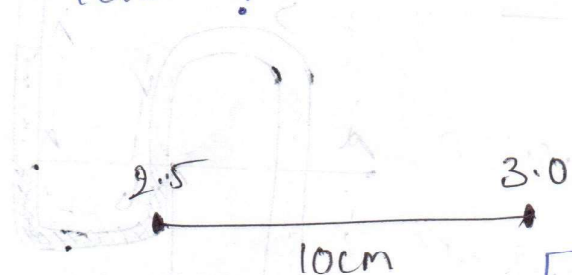
$a_s = v_s \frac{\partial v_s}{\partial s}$
 $= 3 \left(\frac{1}{3} \right)$

$a_s = 1 \text{ m/sec}^2$

$a_n = \frac{v_s^2}{R} = \frac{3^2}{9} = 1 \text{ m/sec}^2$

$a_{\text{total}} = ? \sqrt{a_s^2 + a_n^2} \rightarrow \sqrt{1^2 + 1^2} = \sqrt{2} \text{ m/sec}^2$

9



$a_s = ? \Rightarrow v_s \left(\frac{\partial v_s}{\partial s} \right)$

$= \left(\frac{2.5 + 3.0}{2} \right) \left(\frac{3.0 - 2.5}{0.1} \right)$

$a_s = 13.75 \text{ m/sec}^2$

$a_s = ?$

$v^2 - u^2 = 2as$

$a = \frac{v^2 - u^2}{2s} = \frac{(v+u)(v-u)}{2s}$

$= 13.75$

16

$(u) \vec{V}_s = 3 \sin \theta$

$R = 30m \rightarrow \theta = 45^\circ$

$\rightarrow \alpha_s = ? \Rightarrow \alpha_s = V_s \cdot \frac{\partial V_s}{\partial s}$

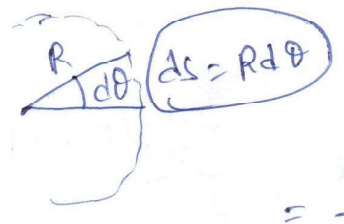
$= 3 \sin \theta \cdot \frac{\partial}{\partial s} [3 \sin \theta]$

$\Rightarrow ds = R d\theta$

$= \frac{3}{R} \sin \theta \frac{\partial}{\partial \theta} [3 \sin \theta]$

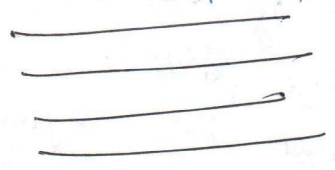
$= \frac{3}{R} \cdot \sin \theta \cdot 3 \cos \theta \Rightarrow \frac{3}{30} \sin 45 \times 3 \cdot \cos 45$

$= \frac{1}{10} + 3 \times \frac{1}{10} \Rightarrow \alpha_s = 1.5 m/s^2$

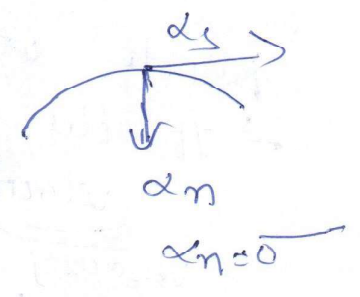
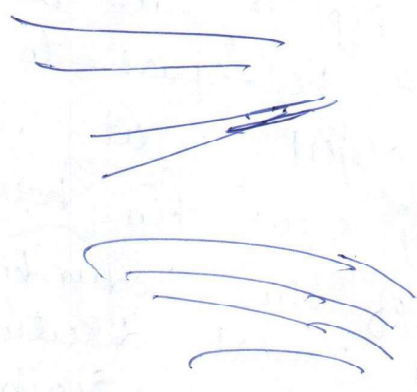


Flow lines

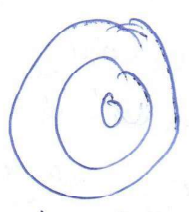
$\alpha_n = 0, \alpha_s = 0$



$\alpha_n = 0, \alpha_s \neq 0$



✓



$\alpha_n \neq 0, \alpha_s = 0$

$\alpha_n \neq 0, \alpha_s \neq 0$