

Con. 10506-12.

KR-5456

(3 Hours)

[Total Marks : 100

**N.B. :** (1) Question No. 1 is **compulsory**.(2) Answer any **four** out of the **remaining** questions.

1. Explain any **four** of the following in brief :- **20**
- Lumped Parameter analysis.
  - Hydrodynamic and Thermal boundary layer.
  - Significance of Nusselt, Reynolds and Grashoff Number in convection heat transfer.
  - Shape factor algebra.
  - Correction factor for LMTD.
  - Fouling of heat exchangers.
2. (a) A 3 mm diameter stainless steel wire ( $K = 20 \text{ W/m}^\circ\text{C}$ ) resistivity,  $P = 10 \times 10^{-8} \Omega\text{m}$ , **10**  
100 meters long has a Voltage of 100 V impressed on it. The outer surface of the wire is maintained at  $100^\circ\text{C}$ . Calculate the centre temperature of the wire. If the heated wire is submerged in a fluid maintained at  $50^\circ\text{C}$ , find the heat transfer co-efficient on the surface of the wire.
- (b) A thermocouple junction is in the form of 8 mm diameter sphere. Properties of **10**  
the material are :  $C = 420 \text{ J/kg}^\circ\text{C}$ ,  $P = 8000 \text{ kg/m}^3$ ,  $K = 40 \text{ W/m}^\circ\text{C}$  and  $h = 40 \text{ W/m}^2^\circ\text{C}$ . This junction is initially at  $40^\circ\text{C}$  and inserted in a stream of hot air at  $300^\circ\text{C}$ . Find (i) Time constant of the thermocouple (ii) the thermocouple is taken out from the hot air after 10 seconds and kept in still air at  $30^\circ\text{C}$ . Assuming the heat transfer coefficient in air  $10 \text{ W/m}^2^\circ\text{C}$ , find the temperature attained by the junction 20 seconds after removing from hot air.
3. (a) What do you understand by critical thickness of insulation ? What is its practical **8**  
significance ? Derive an expression for critical radius of insulation for a spherical surface with usual notations.
- (b) Two long rods of the same diameter one made of brass ( $K = 85 \text{ W/m}^\circ\text{C}$ ) and the **12**  
other made of copper ( $K = 375 \text{ W/m}^\circ\text{C}$ ) have one of their ends inserted into the furnace. Both of the rods are exposed to the same environment. At a distance of 105 mm away from the furnace end, the temperature of the brass rod is  $120^\circ\text{C}$ . At what distance from the furnace end the same temperature would be reached in the copper rod ? Assume the rod to be infinitely long fin. Solve the problem starting from basic differential equation.

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4. (a) Define Buckingham  $\pi$  theorem and derive the following expression for forced convection heat transfer,  $Nu = C(Re)^m (Pr)^n$ . **10**
- (b) An electric wire of 0.25 mm diameter,  $\epsilon = 0.4$  is placed within a tube of 2.5 mm diameter,  $\epsilon = 0.6$  having negligible thickness. This tube in turn is placed concentrically within a tube of 5 mm diameter,  $\epsilon = 0.7$ . Annular spaces can be assumed to be evacuated completely. If the surface temperature of the outer tube is maintained at  $5^\circ\text{C}$ , what must be the temperature of wire so as to maintain the temperature of inner tube at  $120^\circ\text{C}$  ? **10**
5. (a) Derive with usual notations an expression for radiant heat exchange between two infinitely long parallel plane surfaces, assuming the surface to be grey. State the assumptions. **10**
- (b) Air at  $30^\circ\text{C}$  flows with a velocity of 2.8 m/s over a plate 1000 mm (length)  $\times$  600 mm (width)  $\times$  25 mm (thickness). The top surface of the plate is maintained at  $90^\circ\text{C}$ . If the thermal conductivity of the plate material is  $25 \text{ W/m}^\circ\text{C}$ , calculate : **10**  
 (i) Heat lost by the plate, (ii) Bottom temperature of the plate for the steady state condition. The Thermo-physical properties of air at mean film temp. at  $60^\circ\text{C}$  are :  $\rho = 1.06 \text{ kg/m}^3$ ,  $C_p = 1.005 \text{ kJ/kg K}$ ,  $K = 0.02894 \text{ W/m}^\circ\text{C}$ ,  $\nu = 18.97 \times 10^{-6} \text{ m}^2/\text{s}$ ,  $Pr = 0.696$ . Choose the appropriate relation from the following :
- $$\overline{Nu} = 0.664 (Re_L)^{1/2} (Pr)^{1/3} \text{ - for Laminar flow.}$$
- $$\overline{Nu} = 0.036 (Re_L)^{0.8} (Pr)^{1/3} \text{ - for turbulent flow.}$$
6. (a) Derive an expression for LMTD of counter flow heat exchanger. **10**
- (b) A Chemical having specific heat of  $3.3 \text{ KJ/kg K}$  flowing at the rate of  $20000 \text{ kg/h}$  enters a parallel flow heat exchanger at  $120^\circ\text{C}$ . The flow rate of cooling water is  $50000 \text{ kg/h}$  with an inlet temperature of  $20^\circ\text{C}$ . The heat transfer area is  $10 \text{ m}^2$  and the overall heat transfer coefficient is  $1050 \text{ W/m}^2 \text{ K}$ . Find (i) the effectiveness of the heat exchanger (ii) the outlet temperature of water and chemical. Take for water, specific heat is  $4.186 \text{ KJ/kg K}$ . **10**
7. (a) State and explain Fick's law of diffusion. **5**
- (b) Define Schmidt and Sherwood Number with respect to mass transfer. **5**
- (c) An open tank 5.5 m in diameter contains 1 mm deep layer of benzene (molecular weight = 78) at its bottom. The vapour pressure of benzene in the tank is 0.13 bar. The diffusion of benzene takes place through a stagnant air film 2.8 mm thick. The system is operating at 1 atm and  $20^\circ\text{C}$  and under these conditions the diffusivity of benzene is  $8.3 \times 10^{-6} \text{ m}^2/\text{s}$ . Assuming the density of benzene as  $880 \text{ kg/m}^3$  calculate the time taken for the entire benzene to evaporate. **10**